Review Article

Adsorbents for Noxious Gas Sequestration: State of the Art.

ABSTRACT

Adsorbents such as metal organic frameworks (MOFs), polymers, activated carbon (AC) and membranes are becoming prominent for CO_2, SO_2, H_2S and NH_3 capture and in some cases, storage. Using the standard adsorbent properties (SAPs) such as adsorption capacity, selectivity, permeability/permeance, regenerability and reusability, ease of functionability and tunability, thermal and chemical stability etc., suitable candidates for noxious gas sequestration can be determined. In order to foster the development and selection of a more efficient adsorbent, a proper documentation of adsorbent performance in terms of SAPs, is crucial. In this study, a critical review of metal organic framework (MOF), polymer, activated carbon (AC) and membrane adsorbents was performed. Using the SAPs, an up to date comparative analysis was done to select the best performing adsorbents. The results of the comparative analysis were then used to categorize the adsorbents suitability for pre – combustion and post - combustion applications. A perspective of future study on adsorbents for noxious gases sequestration, was also presented.

1. INTRODUCTION

The world's energy demand is continuously increasing with its population growth. A significant part of this energy would be provided by fossil fuels (coal, crude oil and natural). 73.25% of world energy consumption would be provided by fossil fuels by 2040 [1]. Figs. 1 to 3 show global natural gas, crude oil and coal reserves respectively from the years 2016 to 2018, and a projection for production and consumption into the future [2–5]. It is evident from the charts that production and consumption of these fossil fuels would continuously increase into the future (except for coal with a slight reduction). These trends would cumulatively result in the increase in noxious gases released into the atmosphere. These harmful gases such as CO_x, [6], CH_4[7], NH_3, SO_x, NO_x, H_2S [8], Volatile Organic Compounds (VOCs) and volatile organic gases [9] pose a high environmental risk [10]. This therefore necessitates the management of air quality in order to ensure a sustainable environment.
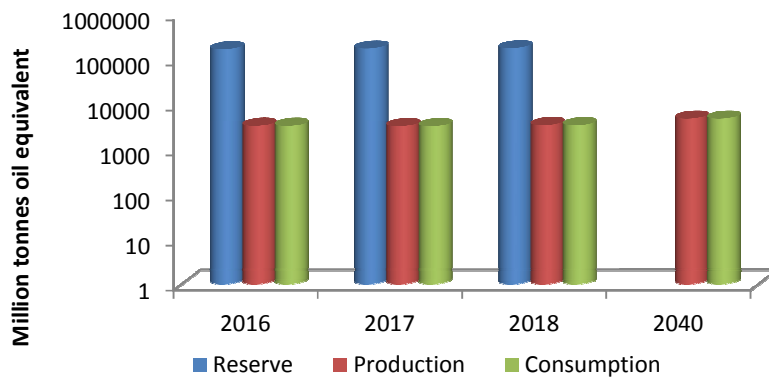
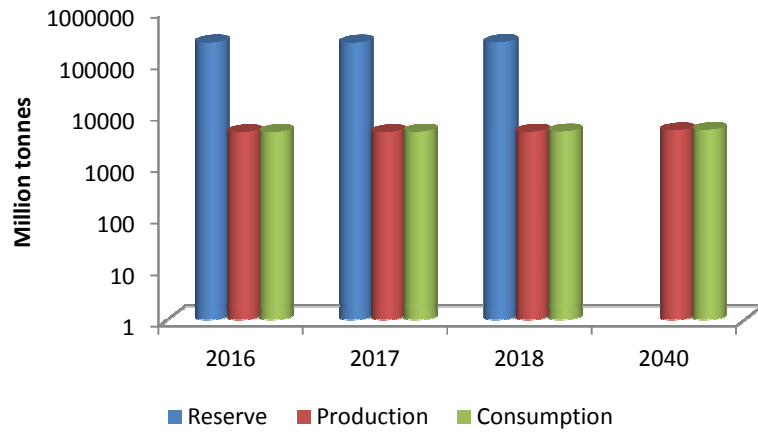**Fig. 1. Natural gas outlook (Source: [2–5])**

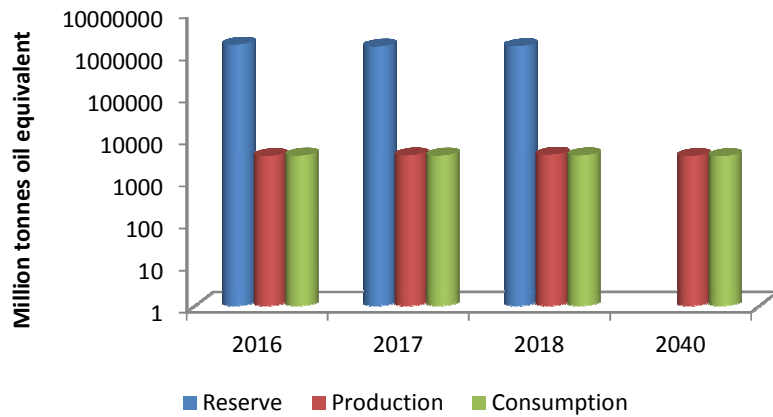**Fig. 2. Crude oil outlook (Source: [2–5])**

Fig. 3. Coal outlook (Source: [2–5])

Different materials and methods [11–18] have been reported for the separation and capture of hazardous gases either from process systems or the environment. Amongst these compounds, adsorbents such as metal organic frameworks (MOFs), polymers, activated carbon (AC) and membranes, have been considered as promising candidates for gas separation and storage, due to their large surface area and pore volume, good thermal and chemical stability, ease of functionability and tunability, low regeneration cost and high selectivity. These adsorbents can be easily modified for specific applications through pre- and post-functionalization of the structure [19–21]. Adsorbent utilization becomes more feasible when its CO_2 adsorption capacity is above 3 mmol/g [22].

For the purpose of this study, an up to date review of the performance of MOFs, polymers, AC and membrane adsorbents are considered. The major focus of this study therefore, was to identify the best performing adsorbents for noxious gas sequestration and then proffer suitable areas for their application.

2. ADSORBENTS FOR CAPTURE OF HARMFUL GASES

Among the numerous types of adsorbents for the capture of harmful gases, MOFs, polymers, membranes and AC are in the forefront of research for harmful gas sequestration as a result of their promising structural properties. *Adsorption, permeability, selectivity, flux rate, reusability and regeneration* are key parameters that determine the deployment of MOFs [21], membranes [23] polymers [24] and AC [25,26] for sequestration of harmful gases in various process systems and conditions. These conditions are imperative for the industrial deployment of these adsorbents for gas capture and storage.

2.1 Metal Organic Frameworks (MOFs)

Metal Organic Frameworks (MOFs) are an emerging class of porous materials constructed from metal-containing nodes and organic linkers [27]. Due to the strong bonds that exist between the metal-containing nodes [also known as secondary building units (SBUs)] and organic linkers, MOFs usually boast of a structure with permanent porosity and open crystalline frameworks as shown in Fig. 4. The organic spacers or the metallic SBUs can be altered to control the pore environment of the MOF [28]. Their inherent characteristics/advantages such as large surface area, ease of functionalization, kinetic diameter, electric properties, Open Metal Sites (OMS), high porosity and tuneable size of pores [29] have made them very attractive compounds in applications such as gas storage and separation, catalysis and sensing [30,31]. The ease with which SBUs and organic linkers are changed and altered has led to the synthesis of thousands of various MOF structures. As a result, the structures and properties of MOFs can be designed and systematically tuned by the choice of building blocks used for the synthesis of the framework [32]. Various strategies have also been reported for improving the performance of MOFs [33].
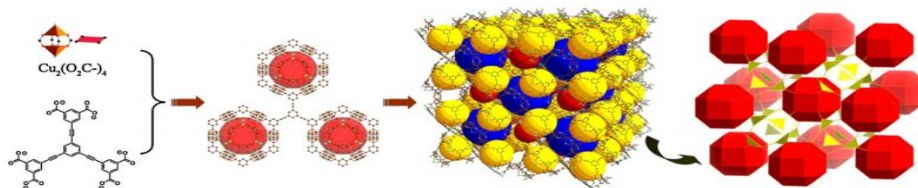
Fig. 4. Crystalline structure of Metal Organic Frameworks [32]

47 MOFs have been investigated for optimization of structure functionality. In this regard, MOFs
48 have been reported to exhibit promising potential for sequestration of gases such as CO_2,
49 H_2S, CH_4, NH_3, NO_x, SO_x etc.[8,14,34–39]. The works of [13,14,40–66] highlight MOFs for
50 CO_2, SO_2, H_2S and NH_3 sequestration at pre- and post-combustion conditions.

2.2. Polymers

Porous Organic Polymers (POP) are composed of organicbuilding blocks connected through
covalent bonds, exhibiting thermal and chemical stabilities, large surface area, ease of
synthesis and low density [67]. There are two classes of POP. They include;

57   i.   Amorphouspolymerswhichcompriseconjugated microporous polymers (CMP)
58   [68], covalent triazine framework [18], porous aromatic framework [18], hyper-
59   cross linked polymers (HCP) [69] and polymers of intrinsic [70]

60   ii. Crystalline polymers(covalent organic polymers) [71].

61 Different polymers have been synthesized for harmful gases sequestration at different
62 process conditions [72] and modification through pre-synthetic and post synthetic
63 functionalization[73] have been reported for improved performance for specific applications
64 [15]. The agents used for functionalization are compounds that increase the affinity of porous
65 polymers for a specific noxious gas. For instance, for CO_2 adsorption, amino functional
66 groups [74], –N heterocycles [75], phenolic motifs [15] are utilized. The method of synthesis
67 plays a key role in the structure of a polymer which invariably affects the adsorption capacity.
68 The different monomers (building blocks) and methods of synthesis are explained by [76].
69 Polymers have also shown excellent reusability [75] and low heat of adsorption[77]. The
70 works of [11,15,18,69,73,78–85] highlight the use of polymers for CO_2, SO_2, NH_3 and H_2S
71 sequestration.

2.3. Activated Carbon (AC)

74 AC has been investigated for capture of noxious gases [86,87]. This is due to reduced cost
75 of production, large surface area, ease of modification of pores, good thermal and chemical
76 stability, hydrophobic nature, stability in the presence of heat and chemical resistance [88].
77 AC shows promising potential for practical applications in terms of balance of performance
78 [89] considering cost of production, benign effect on the environment, availability of
79 precursor materials [90,91] and sustainability [92], and have been reported to exhibit
80 reusability, promising adsorption kinetics [26] and stability after several sorption cycles[63],
81 requiring low regeneration energy [93]. A key determinant to the adsorption performance of
82 AC is the type of precursor used in its synthesis. Different precursors have been reported in
83 the literature for the production of AC.

85 They include bamboo [94], petroleum coke [95], rice husk char [26] wood [96], coconut shell
86 [97], sugarcane bagasse [91], argan fruit shells [98], pinewood shavings char, biochar [89]
87 etc. Amongst these precursors, biochar stands out as it exhibits high porosity and high
88 amount of fixed carbon that can be processed to AC with high micro porosity [89]. Therefore,
89 biochar precursors should receive further investigation in its use for the production of AC for
90 gas sequestration. It is imperative to state that these precursors should have low ash and
91 volatile matter content so as to produce AC with micropores on the surface of the structure
92 for adsorption abilities.

94 AC have been investigated for SO_x and NO_x[99,100], H_2S [101] and CO_2 [100] sequestration
95 at different process conditions. In order to optimize capture and selectivity of AC for specific

96 gases, modification of the structure to increase its affinity for specific gases have been
97 reported [102–108]. Various studies on   the use of AC for CO_2, SO_2, NH_3 and NO_x
98 sequestration, have also been reported [90,91,93,98,108,109].

99 **2.4. Membranes**

100

101 Membranes basically function as filters as shown in Fig. 5. They are used for separation
102 [110]. Different researchers have reported membrane use for capture of harmful gases in
103 literature [17,111,112] as they are environmental benign and efficient in energy consumption
104 [113] and exhibit technical and cost-related merits [114]. Key parameters that determine
105 feasibility of membranes for industrial applications are *permeability and selectivity* [115].
106 Membranes should therefore possess high permeability, permeance, high selectivity, low
107 cost of production and regeneration, good chemical and thermal stability, and ability to resist
108 plasticization [116,117], in order for it to be feasible. Progress in this regard have been
109 recorded in literature where properties of membranes have been optimized even though
110 challenges such as high cost, low physical and chemical stability, low selectivity and low
111 hydrothermal stability still persist [118] . This structure optimization has resulted in the
112 synthesis of different class of membranes [110,119–122].

113

114 Various studies on the use of membrane for the capture of CO_2 and H_2S, have also been
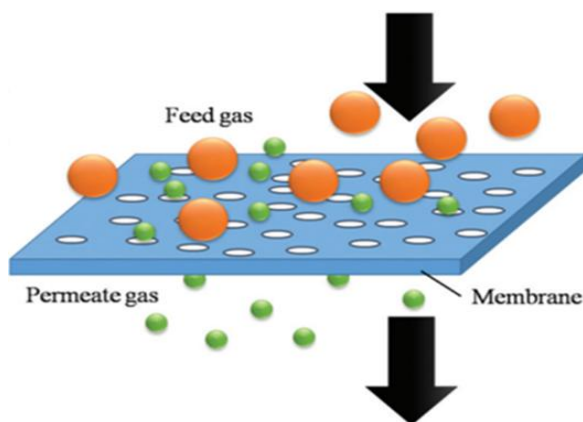115 reported [110,112,122–126].

116

117
118 **Fig. 5. Separation of different molecules using membrane [118]**

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120

121 **3. PERFORMANCE EVALUATION OF ADSORBENTS USING SELECTED SAPS**

122 This section considers the performance of adsorbents reviewed in this study for industrial
123 applications. Although adsorbents for carbon sequestration have not attained the stage of
124 commercial applications [127], they are currently in their demonstration phase. Parameters
125 such as *adsorption capacity, selectivity, permeability/permeance (for membranes),*
126 *regeneration/reusability, thermal and chemical stability,* were used to rank these adsorbents
127 for the purpose of determining the most efficient adsorbent and suitable points for their
128 application. Adsorption capacity was used as the highest-ranking property. Only the best
129 performing adsorbent is reported for each SAP category. The industrial applications
130 considered in this study include pre-combustion and post -combustion conditions.

131

132 **3.1. CO_2 Adsorption capacity at pre-combustion conditions**

133

134 Pre-combustion conditions typically occur at relatively high pressures and low/high
135 temperatures. Such conditions can include process systems such as natural gas, biogas
136 sweetening, etc. Polymers and AC have shown high adsorption capacities at high pressures
137 amongst adsorbents reviewed in this study as highlighted in Table 1. Polymers PPN-4 [128]
138 and PAF-1 [129] exhibited the highest adsorption capacities of 48.20 mmol/g and 29.55
139 mmol/g at pressures of 50 bar and 40 bar respectively at ambient temperatures. ACs LSB3-
140 800 [86] and SBL-PNP-1-4-750 [130] also showed high adsorption capacities of 20.9 mmol/g
141 and 19.65 mmol/g at pressures of 20 bar each at 298K.
142
143 Membranes showed suitability for pre-combustion separation of CO_2 as highlighted in Table
144 2. They have been shown to function within pressure range of pre-combustion carbon
145 capture. Membranes COF 300/6FDA-DAM MMM and COF 300/Pebax MMM [131] can be
146 applied in pre-combustion conditions if their thermal stability at high temperatures is
147 improved.
148
149 MOFs did not show high adsorption capacities as much as polymers and AC for pre-
150 combustion application. The highest performing MOFs for pre-combustion conditions were
151 HKUST-1 and MIL-101 (Cr) [130] with adsorption capacities of 8.07 mmol/g and 7.19 mmol/g
152 at pressures of 10 bar and temperatures of 303K.
153
154 **3.2. CO_2 Adsorption capacity at post-combustion conditions.**
155
156 Post combustion applications occur basically at approximately atmospheric pressure of 1
157 bar and high or low temperatures [132]. At practical post combustion conditions of flue
158 gases from systems such automobiles, petrol generators, motorcycles, gas turbine power
159 plants, oil turbine plants, coal fired plants, water pyrolysis and cement production, only a few
160 adsorbents were found to be applicable as reported in Table 1. Most of the adsorbents
161 showed a decrease in working capacity as temperature increased and ultimately resulted in
162 the decomposition of the structure which implied that the adsorbents cannot be used at
163 relatively high temperature conditions. This can be attributed to the fact that as temperature
164 increases, adsorption capacity of adsorbents such as AC decreases [133]. The low
165 adsorption capacities of AC with values between 0.2 mmol/g to 1.80 mmol/g at 1 bar and
166 373K [104] and that of NORF700 [134] and NCLK3 [135] with adsorption capacities of 2.10
167 mmol/g and 2.00 mmol/g at 1 bar and 323K, support this claim. Polymers, AC and MOFs do
168 not exhibit high adsorption capacities for CO_2 in post-combustion conditions at high
169 temperatures. MOFs 1-een and 1-dmen [136], TAEA modified MIL-101 (Cr) [45] and 1-nmen
170 [136] had the highest adsorption capacities of 5.05 mmol/g, 4.34 mmol/g, 4.05 mmol/g and
171 2.92 mmol/g respectively, at ~1 bar and 313K. Amongst these MOFs, 1-dmen [52] has
172 shown promising potential for practical applications due to its high selectivity of 554 for CO_2
173 in a binary mixture of CO_2/N_2. It is therefore evident that these values for adsorption capacity
174 are not as high as those recorded in pre-combustion conditions as pressure increase results
175 in increase in adsorption capacities [137].
176
177 Most adsorbents showed good adsorption capacities for post combustion CO_2 capture at
178 ambient temperatures, with polymer and AC exhibiting the highest adsorption capacities.
179 Polymer IHBPA (TEPA) [138] and PI-COF-2 [80] had adsorption capacities of 7.65 mmol/g
180 and 5.8 mmol/g respectively at 1 bar and 298K while AC CuO NP-AC [108], ARG-K-Im [98]
181 and DAC-AC-CO_2[98] had adsorption capacities of 6.72 mmol/g, 5.63 mmol/g and 5.52
182 mmol/g respectively at 1 bar and 298K. MOF UTSA-120a [46] was the highest performing
183 MOF in this regard with adsorption capacity of 5.00 mmol/g at 1 bar and 296K, all other
184 MOFs performed below this value in this study. This may be due to the incorporation of
185 functional tetrazine groups into the structure which improved its affinity for CO_2 Considering

186   the working temperatures and pressures of the adsorbents, they are mostly suited for pre-
187   and post - combustion capture at *ambient temperatures.*
188
189
190
191   **3.3. CO$_2$ Selectivity of adsorbents at pre- and post-combustion conditions.**
192
193   In terms of selectivity for CO$_2$ in flue gas stream, MOFs have shown exceptional selectivity
194   that outperformed other adsorbents such as polymers, adsorbents and membranes. This
195   can be attributed to their ease of functionalization using CO$_2$-philic functional groups. MIL-
196   140 [41] and UTSA-120a [46] showed one of the highest selectivity of 1900 and ~600 for
197   CO$_2$ in binary mixtures (CO$_2$/N$_2$). An extremely high selectivity of 7531 for CO$_2$/N$_2$ binary
198   mixture was recorded for MOF MFUM-1(Cu) [139] without information on its adsorption
199   capacity. MOFs 1-dmen [136] and 1-ipen [136] have also been reported to exhibit
200   selectivities of 554 and 273 respectively.
201
202   **3.4. Regenerability and reusability of adsorbents at pre- and post-combustion**
203   **conditions.**
204
205   Some of the adsorbents can be regenerated and re-used for CO$_2$ capture without losing their
206   adsorption capacities. MOF 1-een [136] has been reportedto retain its adsorption capacity
207   after 600 sorption cycles, the highest recorded in this study. Other adsorbents such as AC
208   NSCS-4-700 [63], CNS-AC [90], DAC-AC-CO$_2$[109], polymer (IHBPA (TEPA) [138] and
209   MOFs 1-dmen [52] and 1-een [136] have been shown to retain their adsorption capacities
210   between five to eleven sorption cycles.
211
212   **3.5. Thermal stability of adsorbents at pre- and post-combustion conditions.**
213
214   Polymer CQN-1g [52] had the highest thermal stability at 773K. Other polymer compounds
215   such as TAP-3 [15] and NHC-CAP-1 [75] had thermal stabilities up to 573K and 373K
216   respectively while AC NSCS-4-700 [75] had thermal stabilities up to temperatures of 473K.
217   Some MOFs such as MFM-305 [13], MIL-140 [41] and Cu-Sp5 [140] have been shown to be
218   thermally stable at temperatures of 723K, 573K and 503K respectively. Some adsorbents in
219   this study therefore exhibit thermal stabilities at high temperatures obtainable in most
220   industrial processes. This shows that the adsorbents have potential for use at high
221   temperature conditions. However, literature in this regard remains scarce.
222
223   **3.6. Permeance and selectivity for CO$_2$ of membranes at pre- and post-**
224   **combustion conditions.**
225
226   Membranes have also shown promising permeance and selectivity for CO$_2$ in flue gas
227   mixtures. UiO-66CN@sPIM-1 [120] recorded the highest CO$_2$ permeance amongst reviewed
228   membranes with a value of 12063 Barrer and selectivity (CO$_2$/N$_2$) of 53.5 at atmospheric
229   conditions. MoS$_2$-SILM membrane [141] has been shown to exhibit the highest selectivity of
230   462 for CO$_2$. Also, membranes such as MOF-801/PEBA MMM [141] and COF-5/Pebax [126]
231   with selectivities of 66 and 49.3, respectively for SCO$_2$/N$_2$. Most of the membranes recently
232   synthesized exhibit high CO$_2$ permeance and promising selectivity for CO$_2$ separation which
233   exceeded the standard values for industrial use of 2250 for CO$_2$ permeability and >30 for
234   selectivity. The fact that most membranes have good permeance and selectivity for CO$_2$,
235   makes them well suited for industrial gas separation process applications.

Table 1. Selected CO_2 adsorbents with the highest adsorption capacity.

Material	Adsorbent	CO_2 Uptake (mmol/g)	P (bar)	T (K)	Slcty (CO_2/N_2)	Stability	Cycles of Performance	Potential point of application
PPN-4	Polymer	48.20	50	298	-	-	-	Pre-combustion capture of CO_2
PAF-1	Polymer	29.55	40	298	-	-	-	Pre-combustion capture of CO_2
LSB3-800	AC	20.9	30	298	-	-	-	Pre-combustion capture of CO_2
SBL-PNP-1-4-750	AC	19.65	20	298	-	-	-	Pre-combustion capture of CO_2
SBL-PNP-1-4-750	AC	16.2	20	298	-	-	-	Pre-combustion capture of CO_2
HCP-1	Polymer	13.1	30	298	-	-	-	Pre-combustion capture of CO_2
NSCS-4-700	AC	11.68	8	298	-	-	Showed no loss of adsorption capacity after 10 sorption cycles at 473K regeneration temperature	Pre-combustion capture of CO_2
CNS-AC	AC	8.36	30	303	-	-	Adsorption performance remained unchanged after the 6th sorption cycle	Pre-combustion capture of CO_2
HKUST-1	MOF	8.07	10	303	-	-	-	Pre-combustion capture of CO_2

Material	Type							
IHBPA (TEPA)	Polymer	7.65	1	298	-	Thermal stable up to 363K	Maintained adsorption capacity after 10th sorption cycle.	Post combustion capture of CO_2 at ambient temperatures
MIL-101 (Cr)	MOF	7.19	10	303	-	-	-	Pre-combustion capture of CO_2
CuO NP-AC	AC	6.72	1	298	-	-	-	Post combustion capture of CO_2 at ambient temperature
PI-COF-2	Polymer	5.8	1	298	-	-	-	Post combustion capture of CO_2 at ambient temperature
ARG-K-Im	AC	5.63	1	298	-	-	-	Post combustion capture of CO_2 at ambient temperature
DAC-AC-CO_2	AC	5.52	1	298	28.4	-	Showed stability and maintained its initial adsorption capacity up to 11th sorption cycle	Post combustion capture of CO_2 at ambient temperature; selectivity has to be improved upon for viable applicability
1-een	MOF	5.05 4.04	1 0.15	313	293	-	Working capacity dropped from 13.89wt% to 12.36wt% at the 100th sorption cycle	Sequestration of CO_2 flue gases at post combustion conditions from automobiles, motorcycles, generators etc.

UTSA-120a	MOF	5.00	1	296	~600	-	-	Post combustion capture of CO_2 at ambient conditions due to high selectivity
CQN-1g	Polymer	4.57	1	298	-	Thermally stable up to 773K	-	Post combustion capture of CO_2 at ambient temperatures; Possibility of practical use for CO_2 capture.
1-dmen	MOF	4.34	1	313	554	-	Retained its adsorption capacity after 7th sorption cycle	Post combustion capture of CO_2 from exhaust gas of automobiles, petrol generators, motorcycles etc.
NSCS-4-700	AC	4.27	1	298	-	-	Retained adsorption capacity after 10 sorption cycles at 473K regeneration temperature	Post combustion capture of CO_2 at ambient temperature
TAEA modified MIL-101 (Cr)	MOF	4.06	0.15	313	-	-	-	Post combustion capture of CO_2 from exhaust gas of automobiles, petrol generators etc.
1-ipen	MOF	4.05	1	313	273	-	-	Post combustion capture of CO_2 at ambient temperature

Table 2: CO$_2$ permeance and selectivity capacity of membranes

Material	P (bar)	T (K)	CO$_2$ permeance	CO$_2$/N$_2$	CO$_2$/CH$_4$	Potential point of application
UiO-66-CN@sPIM-1	1.4	298	12063[a]	53.5	-	Separation of CO$_2$ from binary air mixture (CO$_2$/N$_2$) at atmospheric Conditions.
COF 300/6FDA-DAM MMM	8	298	8257[a]	-	75	Pre-combustion separation of CO$_2$
COF 300/Pebax MMM	8	298	8054[a]	-	110	Pre-combustion separation of CO$_2$
TFC#1	3	298	8010[b]	35.8	-	-
TFC#6	3	298	3010[b]	55.7	-	-
FIHM-PEGDME-500-180	3.5	303	1566.8[a]	35.1	-	-
MoS$_2$-SILM	1	293	200[b]	462	-	Post combustion capture of CO$_2$ at ambient temperatures

[a] = Barrer; 1 Barrer = 10^{-10} cc (STP)cm cm^{-2} s^{-1} cmHg^{-2}
[b] = GPU; 1 GPU = 10^{-6} cc (STP)cm^{-2} s^{-1} cmHg^{-1}

3.7. Adsorbent performance for other noxious gases sequestration at pre- and post-combustion conditions.

For NH$_3$ capture at post combustion conditions at ambient temperatures, polymer PCP-1 [142] had the highest adsorption capacity of 22.8 mmol/g as shown in Table 3. MOF Cu$_2$Cl$_2$BBTA [143] and MOF-4 [143] also had good adsorption capacities of 19.79 mmol/g and 17.8 mmol/g respectively. Unfortunately, the thermal and chemical stability of these adsorbents for NH$_3$ capture were not investigated by the authors. Same applies to their regenerability and reusability except for Polymer PCP-1 [142] which showed very low reusability potential due to the reduced number of pores during successive sorption cycles as a result of structure collapse.

MOFs, polymers, AC and membrane have been reported to also sequester noxious gases such as SO$_2$, NH$_3$ and H$_2$S, considerably at pre-combustion and post combustion conditions, despite the chemical stability challenge posed by compounds such as SO$_2$ and H$_2$S to adsorbents. For SO$_2$ capture, MOF compounds such as MOF-3 [56], NH$_2$-MIL-125 (Ti) [144], MFM-300 (Sc) [55] and MIL-160 [144], MOC-1 and MOC-3 [54] had better adsorption

24 capacity at post combustion conditions at ambient temperatures, as shown in Table 4.
25 Unfortunately, none of these compounds were investigated at temperatures consistent with
26 Flue Gas Desulfurization (FGD) systems.
27
28
29 MOF MIL-53 (Al) TDC [57] was found to be the highest performing adsorbent for H_2S
30 capture at post combustion conditions at ambient temperatures, more than Polymers
31 PM_{012}@Ui-66@H_2S-MIPsM [145] and BPP-5 [146] as shown in Table 5. Furthermore,
32 Polymer BPP-5 [146] had a better chemical stability and potential for regenerability and
33 reusability. MOF MIL-101@M-0.5-0.5[147] was found to be the only adsorbent with high
34 potential for H_2S capture at pre-combustion conditions with adsorption capacity of 36.1
35 mmol/g at 10 bar and 298K. Membrane NbOFFIVE-1-NI/6FDA-DAMMMM [146] showed
36 capacity to simultaneously separate CO_2 and H_2S from methane (CH_4), with a selectivity of
37 48 for CO_2+H_2S over CH_4 and a permeance of 950 CO_2+H_2S. This compound has potential
38 for natural gas sweetening if the permeance property is improved.
39
40
41 **Table 3. Selected NH_3 adsorbents with the highest adsorption capacity**
42
43

Material	Adsorbent	NH_3 Uptake mmol/g	P (bar)	T (K)	Cycles of Performance	Potential Point of Applications
PCP-1	Polymer	22.3	1	298	Adsorption capacity reduced at 3rd sorption cycle; Reduction of 5.2 mmol/g between 1st and 2nd sorption cycles was recorded.	NH_3 capture at ambient conditions
Cu_2Cl_2BBTA	MOF	19.79	1	298	-	NH_3 capture at ambient conditions.
MOF-4	MOF	17.8	1	298	-	NH_3 capture at ambient conditions.

44 **Table 4:Selected SO$_2$ adsorbents with the highest adsorption capacity**
45

Material	Adsorbent	SO$_2$ Uptake (mmol/g)	P (bar)	T (K)	Selectivity	Stability	Cycles of Performance	Potential point of application
MOF-177	MOF	25.7	1	293	-	Chemically unstable	-	Not suitable for practical applications.
MOF-3	MOF	10.9	1	298	-	-	-	SO$_2$ capture at ambient conditions.
NH$_2$-MIL-125(Ti)	MOF	10.8	0.95	293	SO$_2$/CO$_2$ – 47-55	-	Showed irreversible adsorption capacity; working capacity reduced at 2nd cycle of performance.	SO$_2$ capture at ambient conditions.
MFM-300(Sc)	MOF	9.4	1	298		-	Adsorption capacity remained unchanged after 10 sorption cycles; regeneration occurred at room temperature.	SO$_2$ capture at ambient conditions
MIL-160	MOF	7.2	0.95	293	SO$_2$/CO$_2$ – 124-128	Thermal and chemical stable	Exhibited good adsorption stability with slight reduction in sorption capacity after 5 sorption cycle	SO$_2$ capture at ambient conditions

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47

Table 5. Selected H₂S adsorbents with the highest adsorption capacity

Material	Adsorbent	H$_2$S Uptake (mmol/g)	P (bar)	T (K)	Stability	Cycles of Performance	Potential point of application
MIL-101@M-0.5-0.5	MOF	36.1 7.63	10 35	298	-	-	Pre-combustion capture of H$_2$S from syngas stream.
MIL-53 (Al)-TDC	MOF	18.1	1	303	Chemically stable in the presence of H$_2$S	Adsorption capacity was retained after 5 sorption cycles; structure exhibits low temperature of 473K for regeneration; regeneration canbe achieved at temp. of 338K.	Integrated Gasification Combined Cycle (IGCC) for H$_2$S capture atambient temperatures
BPP-5	Polymer	17.7	1	298	Superior stability in extremely basic conditions	Author suggested that structure will keep working capacity after various adsorption-desorption cycles	H$_2$S capture at ambient conditions

4. CONCLUSIONS AND PERSPECTIVES

In this review, the performance of selected categories of adsorbents for noxious gas sequestration have been evaluated. The suitability of the adsorbents with the highest SAPs such as adsorption capacity, selectivity, permeance, regenerability and reusability, thermal and chemical stability was determined for pre-combustion and post combustion industrial applications. Perspectives of future studies was also presented.

In terms of adsorption capacity, Polymers, AC and MOFs are suitable for CO_2 adsorption at pre- and post – combustion conditions. Some polymers and ACs were found to have very high adsorption capacities compared to MOFs. MOFs on the other hand, having the highest adsorption capacities are best suited for SO_2 capture. For H_2S and NH_3 adsorption, MOFs and Polymers had the highest adsorption capacity, making them more suitable than ACs.

MOFs have been revealed to show exceptional selectivity for CO_2 and SO_2 in binary mixtures of CO_2/N_2 and SO_2/CO_2 respectively, making it a suitable candidate for CO_2 and SO_2 capture. Most membranes showed selectivity and permeance capacities suitable for industrial applications (>30 for selectivity and >2250 for permeance).

4.1 Perspective for Future Study

Most of the temperature conditions at which these adsorbents were investigated are below practical temperature conditions obtainable in post – combustion process systems. This therefore creates a challenge in their industrial deployment. It is therefore needful to investigate the capture and storage capacities of these absorbent at higher temperatures, so as to ensure their industrial applicability for improved environmental sustainability. Also, information on the selectivity, stability, regenerability and reusability of most of the adsorbents, were not reported. It becomes imperative for these parameters to be properly investigated and reported. The adsorption capacities of MOFs for CO_2, Polymers and ACs for SO_2, as well as ACs for H_2S and NH_3, should be further investigated and improved upon.

COMPETING INTERESTS

Authors have declared that no competing interests exist.

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